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3 Effect of the water-steam phase transition on the electrical conductivity  
4 of porous rocks

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15  
16 **Abstract**

17  
18 The effect of the water-steam phase transition on electrical conductivity was experimentally  
19 investigated in volcanic and sandstone samples to support the interpretation of resistivity data  
20 to determine changes in steam saturation in geothermal reservoirs. The measurements were  
21 performed at simulated in-situ conditions with controlled pore fluid chemistry, temperature,  
22 and confining and pore pressures. At constant temperature (150°C) and confining pressure,  
23 pore fluid was withdrawn from the sample by steadily increasing the volume of the pore fluid  
24 system. At the vapor saturation pressure, the pore water progressively boiled to steam,  
25 resulting in a continuous conductivity decrease by a factor of approximately 20. The study  
26 showed that: (1) for rocks in which conduction is controlled by the pore fluid, the concurrent  
27 changes in both electrical conductivity and pore (vapour) pressure are defined by the pore size  
28 distribution; the changes in liquid-steam saturation are approximately proportional to those in  
29 conductivity and can thus be quantified; and (2) for rocks in which surface conduction is  
30 predominant there is no direct relation between conductivity, pore pressure and drained fluid  
31 volume. This implies that the conduction mechanism controls the pattern of electrical  
32 conductivity variations as steam saturation changes.

33  
34 *Keywords:* Geothermal; Electrical conductivity; Fluid; Phase transition; Basalts; Sandstones;  
35 Iceland

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36 **Nomenclature**

37

38  $k$  = temperature constant (MPa/°C)

39  $p$  = pressure (bar)

40  $p_{pore}$  = pore pressure (bar)

41  $p_{boil}$  = pressure at boiling point of water (vapour pressure) (bar)

42  $p_{cap}$  = capillary pressure (bar)

43  $r$  = rate of volume increase in pore fluid pump (μl/min)

44  $R$  = capillary radius (μm)

45  $t$  = time (h)

46  $T$  = temperature (°C)

47  $T_0$  = reference temperature (°C)

48

49 Greek symbols

50

51  $\gamma$  = surface tension (Pa•m)

52  $\theta$  = wetting angle (°)

53 -----

54 1 bar = 10<sup>5</sup> Pa

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58 **1. Introduction**

59

60 Where pressure in the earth's crust is not high enough to keep water in its liquid phase,  
61 boiling starts and steam<sup>1</sup> fills the pore space instead. This may occur when pore pressures  
62 decrease in response to the withdrawal of fluids from geothermal reservoirs, particularly in  
63 zones that are close to boiling point temperatures and pressures, commonly near the top of  
64 these reservoirs.

65 Because of their high fluid enthalpy, these steam zones (or steam caps) are often well  
66 drilling targets and mapping their expansion is therefore essential. Production well enthalpy  
67 and pressure measurements directly detect phase changes in the fractures that provide well  
68 deliverability. Additionally, there are numerous case histories of the use of precision gravity  
69 and geochemistry measurements to characterize steam saturation change in both the fractures  
70 and the much larger volume of primary (matrix) porosity (Atkinson and Pederson, 1988;  
71 Nicholson, 1993; Hunt and Bowyer, 2007). Repeated conductivity surveys could supplement

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<sup>1</sup> Here we treat the terms “steam” and “vapour” as synonyms regardless of whether the gaseous phase contains liquid droplets or not.

72 such methods. Methods to image the 3D distribution of conductivity in the subsurface to help  
73 geothermal development still need improvement; however, advances in noise reduction and  
74 mapping techniques are being made. In addition, investigations on the magnitude of  
75 conductivity change resulting from pore fluid boiling and related liquid-steam saturation  
76 variations, like the one presented here, are valuable for that purpose.

77 Conduction of electrical current through a volume of porous rock occurs along three  
78 pathways: (1) through the rock matrix, (2) with conductive ions in the pore fluid, and (3)  
79 along the water-rock interfaces in the pores; see Rink and Schoppers (1976), Guéguen and  
80 Palciauskas (1994), and Ruffet et al. (1995) for reviews, and Flóvenz et al. (1985; 2005) for  
81 information on Icelandic rocks. The matrix of both the igneous and sedimentary rocks found  
82 in geothermal systems is not conductive and so the overall rock conductivity is controlled by  
83 pore fluid conduction and interface (surface) conduction. If a dry rock is saturated with  
84 distilled water, its conductivity will typically increase by over three orders of magnitude  
85 (Duba et al., 1978). In addition, geothermal reservoir water usually contains dissolved ions  
86 that increase the fluid conductivity in rough proportion to their concentration. Pores are often  
87 lined with clay minerals that adsorb water and ions, causing high surface conductivity.

88 Many geothermal reservoirs are capped by very conductive, hydrothermally altered clay  
89 zones. Although the types of clay found in high-temperature geothermal systems are much  
90 less conductive, surface conduction related to clay is often an important component of the  
91 bulk conductivity of geothermal reservoir rocks (Boitnott and Hulen, 2001; Flóvenz et al.,  
92 2005; Kulenkampff et al., 2005). The relative contribution of pore fluid conduction increases  
93 under a variety of conditions, for example in reservoirs with higher pore fluid salinity or with  
94 rocks of low clay content.

95 The overall effect of boiling on electrical conductivity within geothermal reservoirs is  
96 poorly constrained by earlier studies although it is expected to decrease once boiling starts.

97 Even though the charge carriers remain in the brine and will enhance the electrical  
98 conductivity of the remaining pore water, the increasing amount of electrically isolating steam  
99 in the pore network reduces the pathways for the electrical current and, hence, decreases the  
100 electrical conductivity. In contrast to this likely scenario for rocks where conductivity is  
101 controlled by pore fluid conduction, the direct effect of boiling on surface conduction in the  
102 pores remains unknown.

103 Some laboratory measurements of electrical conductivity during vaporization of pore fluid  
104 in rock core samples were performed by Roberts et al. (2000; 2001a; 2001b) and Roberts  
105 (2002). They studied rocks of different types and porosities, i.e. andesites (11.5 %) and  
106 hydrothermal breccias (26.8 %) from Awibengkok (Indonesia); metashales ( $3.5 \pm 1.9$  %) from  
107 The Geysers geothermal field (USA); and rhyolitic tuffs (9.0 - 13.5 %) from Fran Ridge and  
108 Yucca Mountain (USA). Their results showed that pore fluid vaporizes gradually as pressure  
109 is decreased and that it occurs at lower pressures than expected from the physical properties of  
110 water alone. Based on the Young-Laplace concept of capillarity (e.g. Bear, 1988), this  
111 observation led Roberts et al. (2001a) to propose a model for a porous medium, where pore  
112 fluid vaporization would be heterogeneous as pore pressure is decreased, because of capillary  
113 suction effects. Accordingly, the phase transition occurs first in the largest pores and then in  
114 consecutively smaller ones. The consequence is that instead of a sharp decrease in electrical  
115 conductivity due to widespread boiling (like that of free water), the conductivity decreases  
116 progressively as vapour forms in more and more pores. For a porous medium, vaporization  
117 occurs when the pore pressure is:

$$118 \quad p_{pore} \leq p_{boil} + p_{cap}, \quad (1)$$

119 where  $p_{pore}$ ,  $p_{boil}$ , and  $p_{cap}$  are the pore, boiling (vapour) and capillary pressures, respectively.  
120 The capillary pressure, by definition, is negative and inversely related to the radius of the  
121 capillary (e.g. Bear, 1988):

122 | 
$$p_{cap} = -2\gamma \cos \theta / R, \quad (2)$$

123 | where  $\gamma$  and  $\theta$  are the surface tension of the wetting fluid and the wetting angle, respectively.

124 | Therefore, for rocks where conductivity is controlled by pore fluid and not by interface  
125 | conduction, the resistivity effects due to an increase in steam saturation will strongly depend  
126 | on the pore microstructure of the reservoir rocks.

127 | A few other studies addressed the effect of steam flooding on the electrical conductivity of  
128 | unconsolidated sands in the context of enhanced oil recovery and soil remediation (Vaughan  
129 | et al., 1993; Butler and Knight, 1995). Despite considerable differences in experimental  
130 | procedures (e.g. non-isothermal conditions) a significant conductivity decrease was observed  
131 | when steam replaced the saline pore fluid. The extent of this decrease was affected by various  
132 | factors such as the chemical composition of the fluid (e.g. the salt content) from which the  
133 | steam was produced, the fraction of vapour within the steam phase (the steam quality), and  
134 | the injection rate.

135 | In this study, we present the first laboratory measurements of changes in electrical  
136 | conductivity during pore fluid vaporization for volcanic rock samples from Icelandic  
137 | geothermal reservoirs. More specifically, the purpose of the present experimental  
138 | investigation was to monitor the electrical conductivity pattern of a water-steam phase  
139 | transition and to establish a quantitative relationship between conductivity and steam  
140 | saturation. In Section 2, the apparatus, the samples, and the fluids used in this investigation  
141 | are described. Also, an outline of the experimental procedure is given. In Sections 3 and 4, the  
142 | experimental results are presented and discussed, respectively. Finally, in Section 5, the  
143 | principal findings of this study are summarized.

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## 147 **2. Experimental setup and procedure**

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### 149 *2.1. Apparatus*

150

151 As in Kristinsdóttir et al. (2007, 2010), the experiments were conducted at the Deutsches

152 GeoForschungsZentrum (GFZ) using a recently installed high-pressure, high-temperature

153 flow-through apparatus. **Figs. 1(a) and (b)** show the general set-up of the apparatus and the

154 mounted specimen assembly, respectively. The apparatus consists of an internally heated oil-

155 medium pressure vessel and a connected pore fluid system. The sample assembly is inserted

156 vertically into the vessel. Both confining and pore pressures are generated with piston-

157 cylinder type syringe pumps. The apparatus allows simultaneous and continuous

158 measurements of permeability, electrical conductivity as well as P- and S-wave velocities.

159 The electrical conductivity is measured with a four-electrode arrangement and a variable

160 shunt resistor. Two silver rings painted onto the samples with a spacing of 25 mm serve as the

161 potential electrodes. At the current electrodes located on the steel plugs facing the sample, the

162 signals are impressed with a function generator (Agilent 33220A). Typically, the voltage is an

163 AC-sine 1.0 V peak-to-peak signal at a frequency of 13 Hz. The input impedance is 10

164 MOhms.

165 The temperature is measured with two PT-100 sensors, one close to the top and one close

166 to the bottom of the specimen, respectively. At 150°C, one notices a temperature difference of

167 approximately 1-2°C along the sample, the topside being the hotter part. A detailed

168 description of the apparatus and specific measurement procedures can be found in Milsch et

169 al. (2008b).

170

### 171 *2.2. Samples*

172 The measurements were carried out on four volcanic rock samples from Iceland, two

173 basalts and two hyaloclastites, and one Fontainebleau sandstone sample (see **Table 1**), each of

174 them cylindrical in shape with 40 mm in length and 30 mm in diameter. The Icelandic  
175 samples were investigated in direct sequel to the electrical conductivity measurements  
176 performed by Kristinsdóttir et al. (2010). In the latter study, these samples were chosen to  
177 investigate the effect of different stages of alteration on the temperature dependence of  
178 electrical conductivity and the respective temperature coefficient; see Revil et al. (1998) and  
179 Kulenkampff et al. (2005) for definitions and Section 4 for details. In contrast, the  
180 Fontainebleau sample was only used in the present study as a reference material and was  
181 heated once to 150°C prior to the start of the experiment.

182

### 183 *2.3. Fluids*

184 As described in Kristinsdóttir et al. (2010), the samples were vacuum-saturated with the  
185 fluids before setting up the specimen assembly. This method also allowed to calculate the  
186 (connected) sample porosity; see Table 1. With the exception of sample K40 which was kept  
187 submerged within the in-situ fluid following drilling, the fluids used in specimens 2B, 3A, and  
188 58 were synthetically prepared. This was done by dissolving reagent grade NaCl, KCl,  
189 Na<sub>2</sub>SO<sub>4</sub>, and K<sub>2</sub>SO<sub>4</sub> salts in distilled water. The specific concentrations chosen were based on  
190 fluid analyses of samples taken at the respective well and reflect the principal in-situ chemical  
191 compositions, except for dissolved non-condensable gases. The resulting electrical fluid  
192 conductivities at 25°C are listed in Table 1. The fluid used for the Fontainebleau sandstone, as  
193 in previous studies (e.g. Milsch et al., 2008a), was a 0.1 molar NaCl standard solution having  
194 an electrical conductivity of 10.8 mS/cm at 25°C.

195

### 196 *2.4. Experimental procedure*

197 During the experiments both temperature  $T$  (nominally 150°C) and confining pressure  
198 (see Table 1) were kept constant while pore pressure was decreased to boil the pore fluid in a



199 controlled manner. The upstream pore fluid pump was stopped and the bypass valve (Fig. 1a)  
200 was opened so that both sides of the sample were connected. The total volume of the pore  
201 fluid system was steadily increased by retracting the downstream pore fluid pump at a  
202 constant rate  $r$  (**Table 2**). As both sides of the sample were connected during this procedure,  
203 the nominal pore pressure was equal at both faces of the specimen. The pore fluid pumps were  
204 kept at room temperature and vaporization was restricted to the hot zone of the pore fluid  
205 system located within the pressure vessel.

206 We emphasize that, in a procedure similar to experiments performed by Roberts et al.  
207 (2001a), (1) we did work without a pressure gradient so that boiling was not restricted to one  
208 end of the sample, (2) we did control the volume flow rate of the pump that was draining fluid  
209 from the sample so that we had a measure of the volume of steam generated in the sample and  
210 also of the resulting pore fluid pressure, and (3) we used a four-electrode arrangement to  
211 measure the electrical properties with potential electrodes on the sample to eliminate electrode  
212 and edge effects. During the experiments the electrical conductivity, the pore pressure, the  
213 volume of the pore fluid pump, as well as the sample temperature were continuously  
214 monitored.

215

### 216 **3. Results**

217

218 **Fig. 2** displays the raw experimental data as a function of time. The shaded area shows the  
219 pressure range corresponding to the boiling point of water for the 145-150°C temperature  
220 range. The pore fluid pumps that were used had a maximum pressure rating of 50 MPa. The  
221 specifications report a resolution of  $\pm 0.25$  MPa and a zero pressure drift of  $\pm 0.13$  MPa in 48  
222 hours at constant temperature. Due to these restrictions and in contrast to electrical  
223 conductivity, the accuracy of determining the vapour pressure at a given temperature is  
224 limited. Furthermore, fluctuations in sample temperature by up to  $\pm 1^\circ\text{C}$  and an apparently

225 correlated variation in pore pressure of 0.1-0.2 MPa/°C occurred at some stages of the  
226 experiment. This was much greater than the almost linear 0.012 MPa/°C variation in pressure  
227 that would be expected at the boiling point in the 145-150°C temperature range. In fact, these  
228 temperature and pressure fluctuations are indirectly related to each other and represent  
229 experimental artefacts that originate from laboratory temperature variations.

230 In previous experiments (e.g. Milsch et al., 2008a; 2008b) we noticed that changes in  
231 sample temperature  $T$  as measured with the two PT-100 sensors mentioned in Section 2.1 are  
232 related to a signal drift of the thermocouple actively controlling the heater whose electrical  
233 connector is located outside the pressure vessel. Similarly, changes in pore pressure are a  
234 consequence of an electronic drift of the pressure gauge, which is exposed to the atmosphere,  
235 and do not represent the true situation within the pore space of the sample. In these  
236 experiments we also observed that variations in laboratory temperature yielded a linear  
237 relationship between the temperature changes  $\Delta T$  within the pressure vessel and the erroneous  
238 variation of the pressure gauge read-out  $p_{pore}$ . This effect had to be removed from the data to  
239 reveal the true pore pressure variations in the course of an experiment. Consequently, we  
240 applied a linear correction that relates the true temperature variations as measured within the  
241 vessel to apparent changes in pore pressure:

$$242 \quad p_{pore}(T) = p_{pore}(T_0) + k(T - T_0), \quad (3)$$

243 where  $p_{pore}$ ,  $T$ ,  $T_0$ , and  $k$  are the pore pressure, sample temperature, reference temperature, and  
244 some temperature constant, respectively.

245 The reference couple [ $p_{pore}(T_0)$ ,  $T_0$ ] refers to the particular point in the pressure graphs of  
246 Fig. 2 where the pore pressure remained constant for the first time, indicating the onset of  
247 boiling (Section 4). The reference pressure  $p_{pore}$  was then determined as the tabulated vapour  
248 pressure corresponding to the reference temperature  $T_0$  (e.g. Lemmon et al., 2005). The  
249 temperature constant  $k$  was determined from significant short-time variations of both

250 temperature  $T$  and pore pressure  $p_{pore}$  that could unequivocally be attributed to changes in  
251 laboratory temperature (e.g. sample 58 between 17.5 and 18.5 h). The values of  $k$  differed  
252 slightly from one experiment to another; see Table 1.

253 The result of this correction is shown in **Fig. 3**, which displays the pore fluid pressure as a  
254 function of time together with the observed electrical conductivity changes, the sample  
255 temperature, and the fluid volume drained from the sample. The total electrical conductivity  
256 decrease during vaporization was generally 1 to 2 orders of magnitude and thus significant.  
257 Except for sample 58 where the measurement was terminated earlier, the electrical  
258 conductivity ultimately reached a minimum. For sample 2B, the pronounced conductivity  
259 increase after 85 h remains unexplained.

260 For better visibility and for documentation, **Fig. 4** displays the corrected pore pressure of  
261 each sample as a function of the volume change within the pore fluid system. The graphs  
262 illustrate that, for all samples, there was a discontinuous decrease in pore pressure. Initially, as  
263 the volume of the pore fluid system is increased, the pressure dropped rapidly due to elastic  
264 relaxation. Then, at the boiling point, an approximately constant pore pressure level was  
265 maintained. Finally, the pore pressure started to decrease again. Both the volumetric onset and  
266 the extent of this second pore pressure decrease were sample-dependent.

267

#### 268 **4. Discussion**

269

270 In this section we will interpret the observed, sample-dependent electrical conductivity  
271 (Fig. 3) and pore pressure (Fig. 4) patterns with respect to drained pore fluid volume, steam  
272 saturation, and predominant conduction mechanism.

273 In our experiments, the fluid started to boil once the vapour pressure corresponding to the  
274 highest temperature within the pore fluid system was reached. The fluid was then in a state of  
275 liquid-steam equilibrium at constant pore pressure as long as liquid at that temperature

276 remained. The principal decrease in electrical sample conductivity did not occur  
277 instantaneously after the boiling pressure was reached (Fig. 3). We attribute this delay to the  
278 initial vaporization of the free water inside the pore fluid system, before the onset of  
279 significant boiling in the sample. Sometimes (e.g. samples 3A, FTBS12, and eventually 2B), a  
280 smaller and transient electrical conductivity decrease was observed, followed by a  
281 conductivity plateau. This observation is consistent with two different interpretations, either  
282 (A) it was related to fluid boiling in the internal tubing and end caps of the assembly that cuts  
283 off the residual current through the outer fluid capillaries, or (B) it was related to pore fluid  
284 vaporization within the sample above the upper potential electrode. Due to the variability of  
285 this effect from sample to sample, interpretation (B) is more likely to be correct and the  
286 occurrence or absence of a conductivity plateau can be attributed to slight variations in the  
287 temperature gradient along the sample. When fluid was continuously drained from the  
288 sample, ultimately, a progressive decrease in electrical sample conductivity followed until the  
289 latter reached a distinct minimum (Fig. 3).

290 The decrease in pore pressure at later stages of each experiment (Fig. 4) can be explained  
291 by (A) temperature gradients along the specimen, (B) variations in the pore radii of an  
292 individual sample as described by Roberts et al. (2001a), and/or (C) expansion of steam after  
293 all liquid at 150°C has been vaporized. With respect to (A), the minimum pore pressure  
294 observed was approximately 0.2 MPa corresponding to a vaporization temperature of only  
295 120°C, which is inconsistent with the experimental conditions. As long as there is liquid left  
296 to vaporize and if the rate at which the volume of the pore fluid system is increased is low  
297 enough so that the equilibrium pressure can be maintained by steam production - which  
298 evidently was the case in all experiments (Fig. 4) - it is reasonable to inquire if the observed  
299 decrease in pore pressure is because of a vapour pressure drop due to capillarity (case B).

300 The relationship between variations in both electrical conductivity and pore (vapour)

301 pressure with respect to the drained fluid volume was observed to be sample-dependent.

302 Disparities in the pore pressure change pattern would then reflect differences in sample

303 microstructure with respect to the distribution of individual pore radii; i.e.,

304 (I) For samples 2B, 3A, and FTBS12, the pore pressure started to decrease after the  
305 electrical conductivity had dropped by about 90 %, evidence of both large pores  
306 and a narrow pore radius distribution.

307 (II) For sample K40, the pore pressure started to decrease after the conductivity had  
308 dropped by approximately 50 %, indicating the predominance of one narrow pore  
309 size class larger than the remaining pores that have a broad pore radius  
310 distribution.

311 (III) For sample 58, both electrical conductivity and pore pressure initially showed a  
312 concurrent decrease followed by a continuous drop in conductivity at constant  
313 vapour pressure (Fig. 3, after 19 h). This suggests a broad pore radius distribution  
314 and the existence of one narrow class of smaller pores.

315 For the Fontainebleau sandstone interpretation (I) is in agreement with mercury porosimetry  
316 measurements performed by Milsch et al. (2008a). The pore radius distribution in this rock is  
317 very narrow, with 90 % of porosity accounted for by pores with radii between 4 to 10  $\mu\text{m}$ . For  
318 the Icelandic samples these data are not yet available. However, if capillarity is solely  
319 responsible for the observed decrease in pore pressure, the above scenarios are consistent.

320 Following the procedure in Roberts et al. (2001a) we calculated the minimum pore  
321 (capillary) radius  $R$  related to vaporization by the maximum capillary pressure observed ( $p_{cap}$   
322  $\approx 0.25$  MPa at  $150^\circ\text{C}$ ); we assumed a surface tension of the wetting fluid (water) of  $5.2 \cdot 10^{-3}$   
323 Pa $\cdot\text{m}$  (Weast, 1984) and a wetting angle of about zero. From Eq. (2) one obtains  $R \geq 42$  nm,  
324 which indicates that virtually all pore size classes were affected by vaporization in the present  
325 experiments.

326 One important conclusion that can be drawn from the outcome of the experiments is the  
327 amount of drained fluid necessary to reduce the electrical conductivity to a minimum in  
328 relation to the individual sample porosity. To compare the electrical conductivity history of all  
329 samples as a function of the pump volume increase, we performed a conductivity  
330 normalization with respect to the starting values (Fig. 3); the results are shown in **Fig. 5**.

331 In all experiments  $5 \pm 1$  ml of fluid had to be drained before the electrical conductivity of  
332 the sample became affected. This volume relates directly to the free fluid volume (e.g. in  
333 tubings) located inside the pressure vessel. The different starting values for volume change in  
334 Fig. 5 reflect the uncertainty in picking the correct sample related electrical conductivity  
335 decrease from Fig. 3. Except for sample 58, the observed conductivity patterns are similar.  
336 The electrical conductivity decreased to about  $5 \pm 1$  % of its starting value. Furthermore  
337 (excluding sample 58),  $7 \pm 2$  ml of fluid had to be drained from the sample until the minimum  
338 electrical conductivity was reached.

339 The (connected) pore volume between the potential electrodes was 2.2 (FTBS12), 2.3  
340 (K40), 2.6 (2B), 3.5 (58), and 3.7 (3A)  $\text{cm}^3$ . The total (connected) pore volume of the samples  
341 was 3.5 (FTBS12), 3.7 (K40), 4.1 (2B), 5.7 (58), and 5.9 (3A)  $\text{cm}^3$ . Finally, the drained fluid  
342 volume at the conductivity minimum was approximately 5.1 (FTBS12), 9.2 (K40), 5.5 (2B),  
343 17.7 (58), and 6.0 (3A) ml. The drained fluid volume for sample 58 follows from a linear  
344 extrapolation of the respective graph in Fig. 5.

345 As vaporization proceeded concurrently both between and outside the potential electrodes  
346 and fluid was drained from all parts of a sample, the ratio between the drained fluid volume  
347 and the pore volume is 1.5 (FTBS12), 2.5 (K40), 1.3 (2B), 3.1 (58), and 1.0 (3A), hence  
348 approximately  $2.0 \pm 1.0$  times the relevant pore volume. Due to condensation outside the  
349 vessel the drained fluid volume in fact directly reflects the vaporized liquid volume contained  
350 within the pore space of a sample.

351 The ratio between the drained fluid volume and the total pore volume allows a  
352 classification of the rocks based on the normalized conductivity graphs in Fig. 5. Samples 3A,  
353 2B, and FTBS12 display very similar conductivity patterns. Here, every part of the drained  
354 volume larger than the pore volume can be attributed to smaller pores and/or a broader pore  
355 size distribution as the excess volume reflects the vapour expansion related to a pressure  
356 decrease necessary for further vaporization. For example, 4.0 ml of fluid had to be drained  
357 from sample 3A to reduce the electrical conductivity by 90 % at constant pore pressure.  
358 Withdrawal of an additional 2.0 ml was necessary to attain the conductivity minimum by a  
359 concurrent decrease in pore pressure. For this sample, the drained fluid volume exceeded the  
360 total pore volume by only a small amount (0.1 ml). For sample 58, in contrast, the excess  
361 volume at the conductivity minimum was comparatively large. This suggests that the curve  
362 shapes in Fig. 5 could also be indicative of the respective dominant conduction mechanism as  
363 vaporization proceeds.

364 Electrical conduction in sample FTBS12 is definitely controlled by the pore fluid for the  
365 given fluid salinity (Milsch et al., 2008a). The same argument applied to samples 3A and 2B  
366 indicates that conduction during vaporization in hyaloclastites originating from the chlorite  
367 alteration zone should be controlled by the pore fluid as well, even for pore fluids of low  
368 salinity as those used in the present study. Sample K40, a basalt containing mixed-layer clays,  
369 displays a transition from pore fluid to surface conduction at a later vaporization stage.  
370 Finally and for the present fluid composition, conduction in sample 58, a basalt from the  
371 smectite alteration zone, is expected to be mainly surface controlled. In this case, the decrease  
372 in electrical conductivity upon continuous fluid drainage should be related to some  
373 progressive destruction of the conductive layer on the mineral surfaces rather than to the  
374 phase transformation within the pore space itself. Here, the correlation of electrical  
375 conductivity and pore pressure patterns is more complex; case (C) mentioned earlier. This

376 interpretation regarding differences in the predominant conduction mechanism for the present  
377 fluid-rock combinations is supported by a comparison of the conductivity temperature  
378 coefficients reported by Revil et al. (1998) with the ones measured by Kristinsdóttir et al.  
379 (2010): 0.023 1/°C for pore fluid conduction and 0.040 1/°C for interface conduction  
380 compared to 0.027 1/°C for samples 2B and 3A, 0.030 1/°C for sample K40, and 0.067 1/°C  
381 for sample 58, respectively.

382 A variety of conductivity models exist (e.g. Glover et al., 2000 and references therein) that  
383 extend Archie's Law (Archie, 1942) to more than one pore fluid phase. The correct  
384 application of such models requires the most probable distribution of the respective fluid  
385 phase to be known, which in the present study is very uncertain. However, if boiling occurs in  
386 thermodynamic equilibrium with the pore pressure decrease being controlled by capillarity, it  
387 is likely that vapour bubbles of progressively decreasing size are homogeneously distributed  
388 throughout the pore space of a sample. Taking sample FTBS12 as a reference, we conclude  
389 that at a maximum drained volume of approximately 1.5 times the pore volume, the free  
390 liquid contained within the pore space has been transformed into vapour. Consequently, for all  
391 samples where conduction is primarily related to the pore fluid, the electrical conductivity  
392 signal approximately reflects the respective liquid or steam saturation at a given stage of  
393 vaporization.

394

395 |

## 396 **5. Conclusions**

397

398

399 A high-pressure, high-temperature flow-through apparatus was used to perform electrical  
400 conductivity measurements under controlled  $p$ - $T$  conditions during the water-steam phase  
401 transition in porous rocks from Icelandic hydrothermal reservoirs. In addition, one sample of  
402 Fontainebleau sandstone was studied as reference material.

402 The pore fluid vaporized at pressures equal to or below that of the boiling point of free



403 water at the respective temperature. After the onset of vaporization within the pore space, the  
404 electrical conductivity of the samples decreased continuously by a factor of approximately 20  
405 until reaching a distinct minimum.

406 For rocks with conduction primarily controlled by the pore fluid, the qualitative  
407 application of the capillarity model proposed by Roberts et al. (2001a) yields a reasonable  
408 interpretation of the observed concurrent variations of both electrical conductivity and pore  
409 (vapour) pressure with respect to the pore size distribution. Based on the measured capillary  
410 pressure, that model predicts that the decrease in electrical conductivity is associated with  
411 boiling in virtually all pore size classes.

412 For two out of five samples, withdrawal of significant excess fluid volumes was necessary  
413 to minimize electrical conductivity; thus implying that there is no direct relation between  
414 conductivity, pore pressure and drained fluid volume in rocks where surface conduction  
415 predominates. Therefore, it is concluded that the conduction mechanism controls the pattern  
416 of electrical conductivity variations as vaporization proceeds.

417 The experimental results also suggest that, at the observed conductivity minimum, all  
418 samples can be considered dry, apart from retained water on grain surfaces or in ultra-small  
419 pores. Consequently, if the bulk conductivity of the rock is controlled by pore fluid  
420 conduction, then changes in liquid-steam saturation can be characterized based on measured  
421 changes in rock conductivity. Otherwise, if surface conduction predominates or if the  
422 conduction mechanism is variable during vaporization, changes in steam saturation cannot be  
423 quantified by conductivity measurements and the exact phase distribution of steam is  
424 unknown.

425 In future investigations, priority should be given to studies that address: (1) the effect of  
426 dissolved gases on conductivity during vaporization, as many geothermal reservoir fluids  
427 contain significant amounts of gas, mainly CO<sub>2</sub>, especially in the shallow parts of the

428 reservoir likely to develop a steam cap; (2) the quantitative relationship between the clay  
429 mineralogy and content and the conductivity patterns observed in the present study; and (3)  
430 the liquid-steam phase distribution within the pore space as boiling proceeds.

431

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433

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439

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## 520 **Figure captions**

521 **Fig. 1. (a)** General set-up of the experimental apparatus used in this study. (1) downstream  
522 pore fluid pumps; (2) reservoirs for fluid sampling; (3) pressure vessel with internal heater  
523 and specimen assembly; (4) confining pressure pump; (5) upstream pore fluid pumps; (6)  
524 fluid reservoir. **(b)** Details of the mounted specimen assembly.

525

526 **Fig. 2.** Main results of the pore fluid vaporization experiments - raw data: Changes in  
527 electrical conductivity (blue), temperature (red), volume in pore fluid pump (black) and pore  
528 pressure (as measured in pump; green) with time. The shaded area shows the (vapour)  
529 pressure at which water boils for  $T = 145\text{-}150^\circ\text{C}$ . Note that there is a break in the pore  
530 pressure axis for all graphs. In the plot labeled "Sample 3A (begin)", only the first 30 hours of

531 the experiment are shown to highlight early time variations. See Section 3 for more details.

532

533 **Fig. 3.** Main results of the pore fluid vaporization experiments - pore pressure corrected  
534 according to Eq. (3): Changes in electrical conductivity (blue), temperature (red), volume in  
535 pore fluid pump (black) and pore pressure (as measured in pump; green) with time. The  
536 shaded area shows the (vapour) pressure at which water boils for  $T = 145-150^{\circ}\text{C}$ . Note that  
537 there is a break in the pore pressure axis for all graphs. For sample 3A the first 30 hours of the  
538 experiment are highlighted in plot “Sample 3A (begin)”. See Section 3 for more details.

539

540 **Fig. 4.** Corrected pore pressure (Eq. 3) as a function of the volume increase in the pore fluid  
541 system. The shaded area shows the (vapour) pressure at which water boils for  $T = 145-150^{\circ}\text{C}$ .  
542 Note that there is a break in the pressure axis for all samples except sample 58. See Section 3  
543 for more details.

544

545 **Fig. 5.** Normalized electrical conductivity as a function of the volume increase in the pore  
546 fluid system. For each sample, the conductivity normalization was performed using the  
547 respective starting conductivity immediately before the initiation of boiling within the pore  
548 space as determined from Fig. 3. See Section 4 for more details.

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554 **Figures**

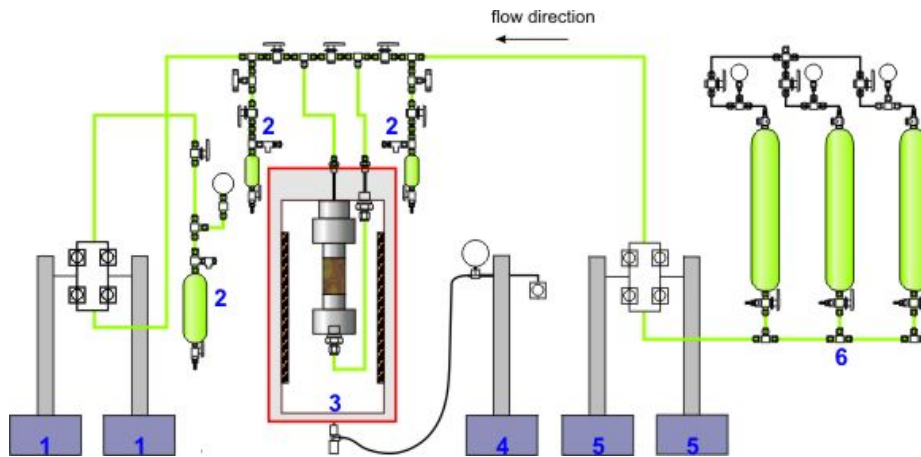
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557 Figure 1a

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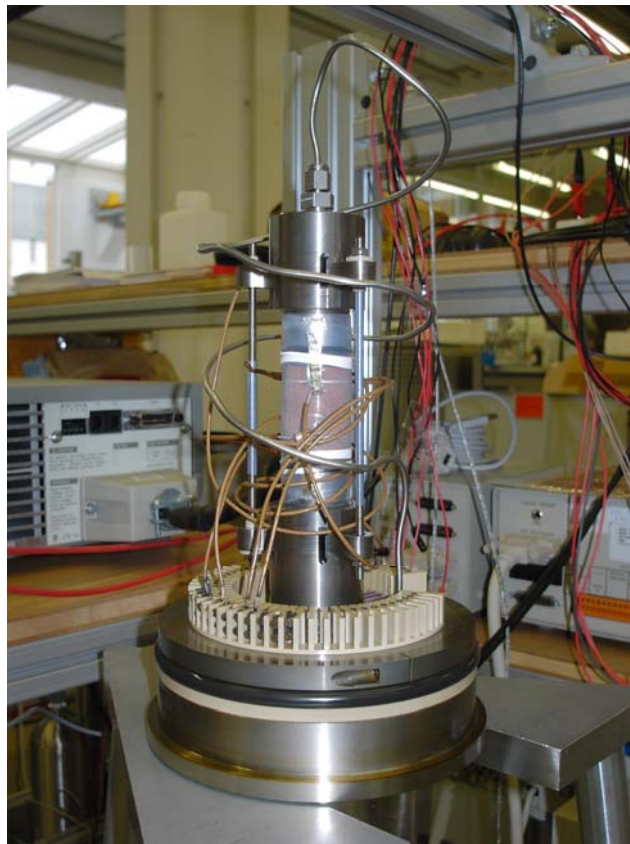
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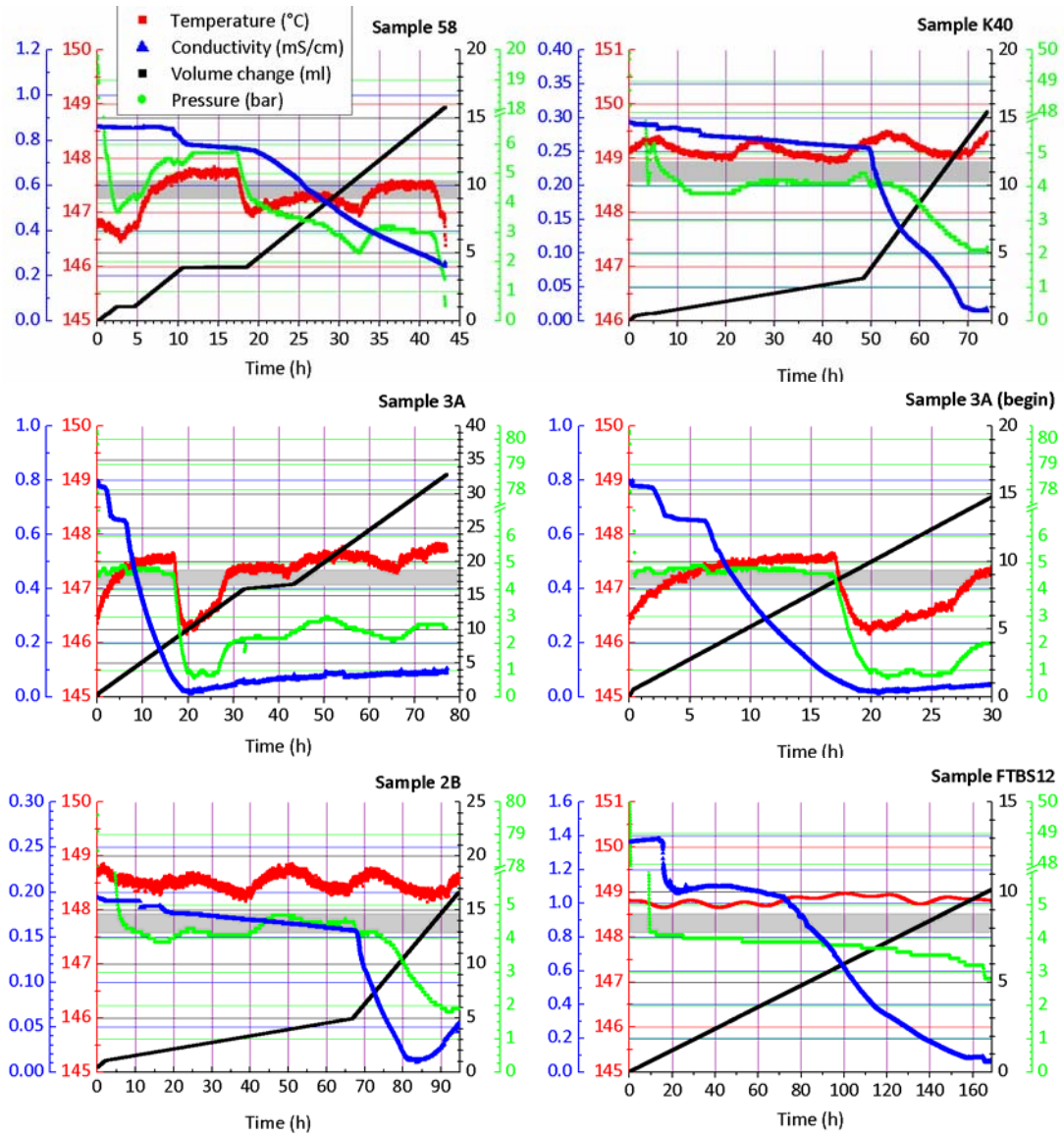
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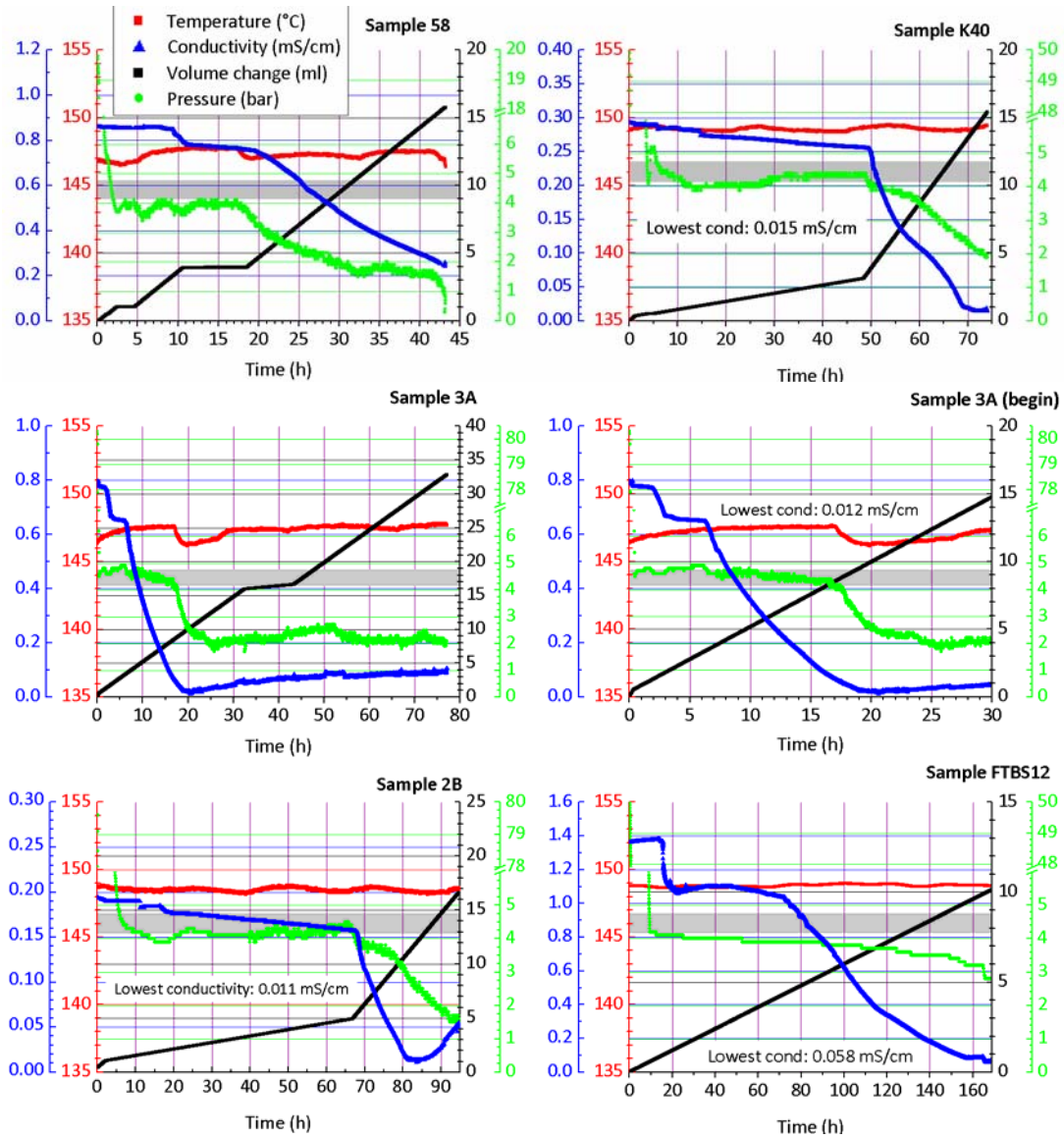
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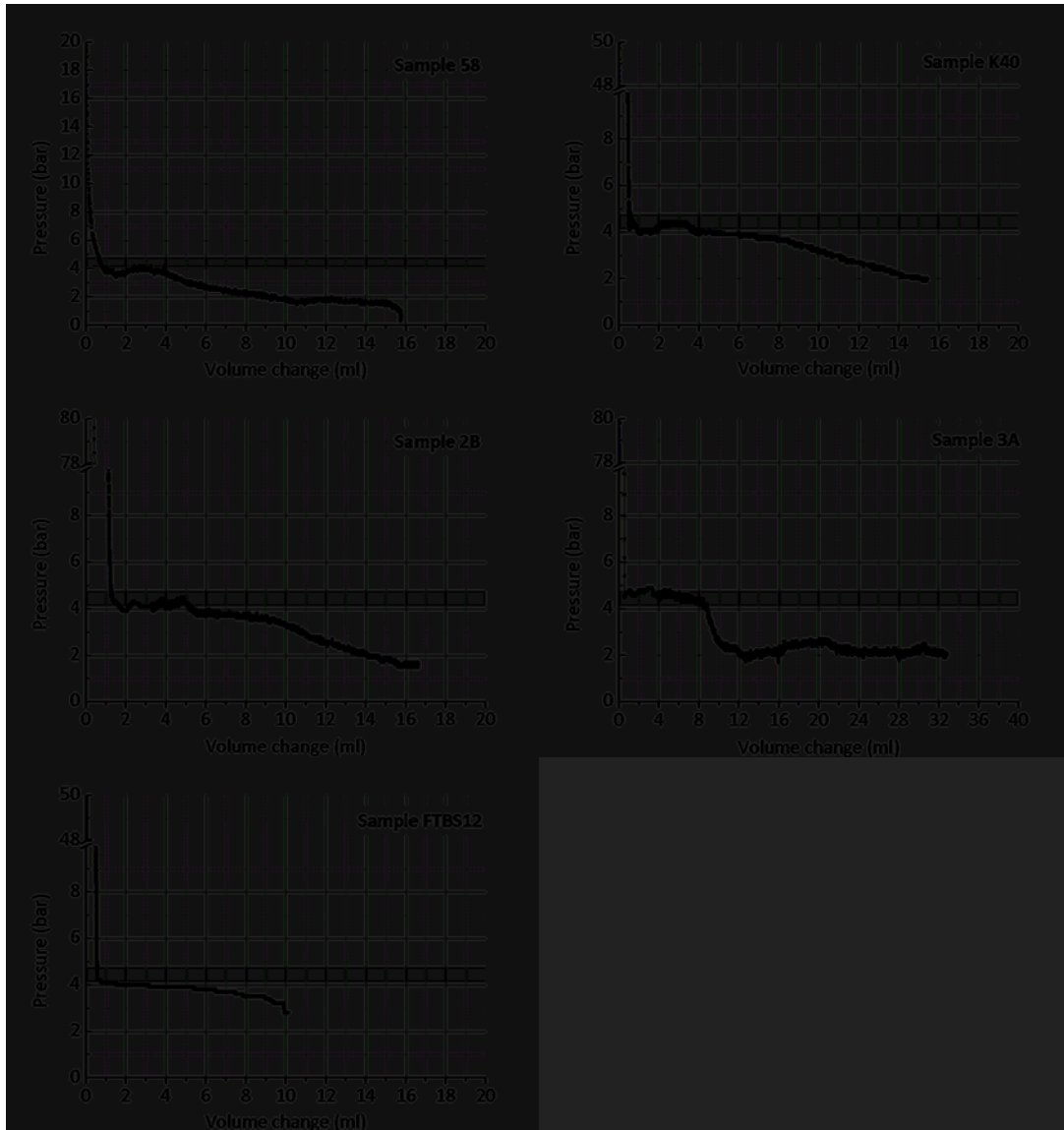


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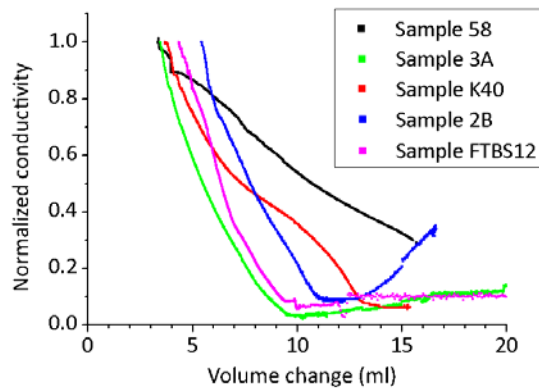


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611 Figure 4  
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617 Figure 5  
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620 **Tables**

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Table 1  
Sample characteristics

Sample No.	Sampling location	Well No.	Year of sampling	Rock type	Hydrothermal alteration	Sample depth (m)	In-situ temperature (°C)	Estimated in-situ fluid conductivity at 25°C (mS/cm)	Porosity (%)	Density (g/cm <sup>3</sup> )	Confining pressure (MPa)	Year of measurements	Temperature constant <i>k</i> (MPa/°C)
2B	Hengill	ÖJ-1	1994	Hyaloclastite	Chlorite / Epidote	794.5	200	0.808	14.6	2.59	18.5	2007	0.10
3A	Hengill	ÖJ-1	1994	Hyaloclastite	Chlorite / Epidote	795.0	200	0.808	20.7	2.46	15.0	2006	0.15
K40	Krafla	KH-5	2006	Basalt	MLC / Chlorite	537.5	120	---	13.2	2.29	13.5	2007	0.10
58	Krafla	KH-1	1991	Basalt	Smectite / MLC	187.5	~160	0.780	20.0	2.37	5.0	2006	0.15
FTBS12	Fontaine-bleau	N/A	2005	Sandstone	None	(0)	(20)	(10.8)	12.5	2.29	10	2007	0

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628 MLC: Mixed-layer clays

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Table 2  
Rate of volume increase  $r$  in the downstream pore fluid pump during vaporization

Sample No.	Rate of volume increase $r$ ( $\mu\text{l}/\text{min}$ )	Time interval $t$ (h)
2B	5	0 - 2
	1	2 - 67
	7	67 - 94.5
3A	25	0 - 0.3
	8	0.3 - 32.5
	1	32.5 - 43.5
	8	43.5 - 77
K40	5	0 - 1
	1	1 - 4
	0	4 - 5
	1	5 - 48.3
	8	48.3 - 74
58	8	0 - 4
	0	4 - 6.5
	8	6.5 - 10.5
	0	10.5 - 18.5
	8	18.5 - 43
FTBS12	1	0 - 169

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